

Modeling Pulsed Air Sparging Mass Removal of DNAPL on a Lab Scale using a Dual-Media Approach

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Overview

- ★ Objectives
- ★ Previous Modeling Attempts
- ★ Lab Experiment
- ★ Single Domain Results
- ★ Dual Domain Approach and Results
- ★ Summary

Objectives

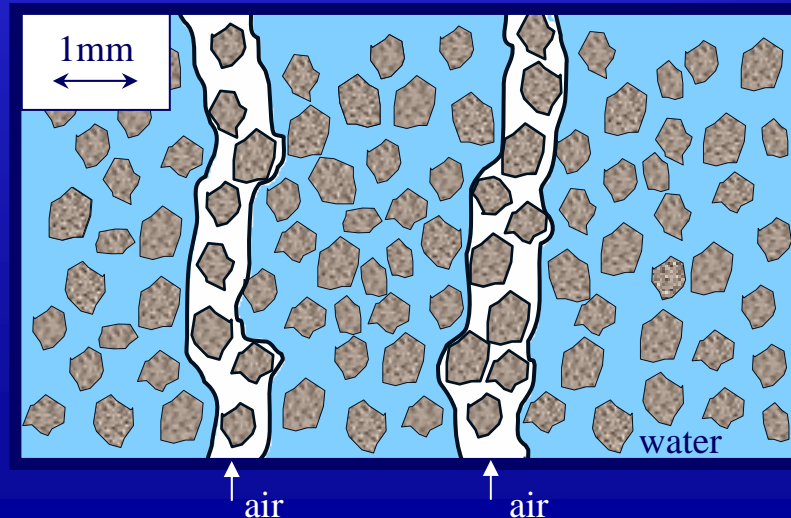
- ★ Obtain a better understanding of contaminant mass removal in air sparging
 - Rate-limited mass transfer effects
 - Pulsed Air-Sparging
- ★ Validate multiphase fluid flow model T2VOC for predicting contaminant mass removal

T2VOC Code

- ★ Developed from TOUGH Codes at U.C. Berkeley
(transport of **u**nsaturated **g**roundwater and **h**eat)
- ★ 3-d numerical simulator for multiphase flow and transport of organic chemicals in variably saturated media

Previous Modeling Attempts

- ★ Conventional multiphase flow approaches have accurately modeled the sparge gas plume*
 - Large scale heterogeneities can be accounted for: *i.e. capillary and permeability barriers*
 - Local effects not resolved: *important controls on mass transfer and removal*
 - Local chemical equilibrium assumption: *can overestimate interphase mass transfer*



*(Hein et al., 1997; McCray and Falta, 1997)

Previous Modeling Attempts

★ Interphase mass transfer has been accounted for in some codes*

- These models do not account for transient 2D or 3D multiphase flow that occurs during air sparging
- Use conventional first order mass transfer:

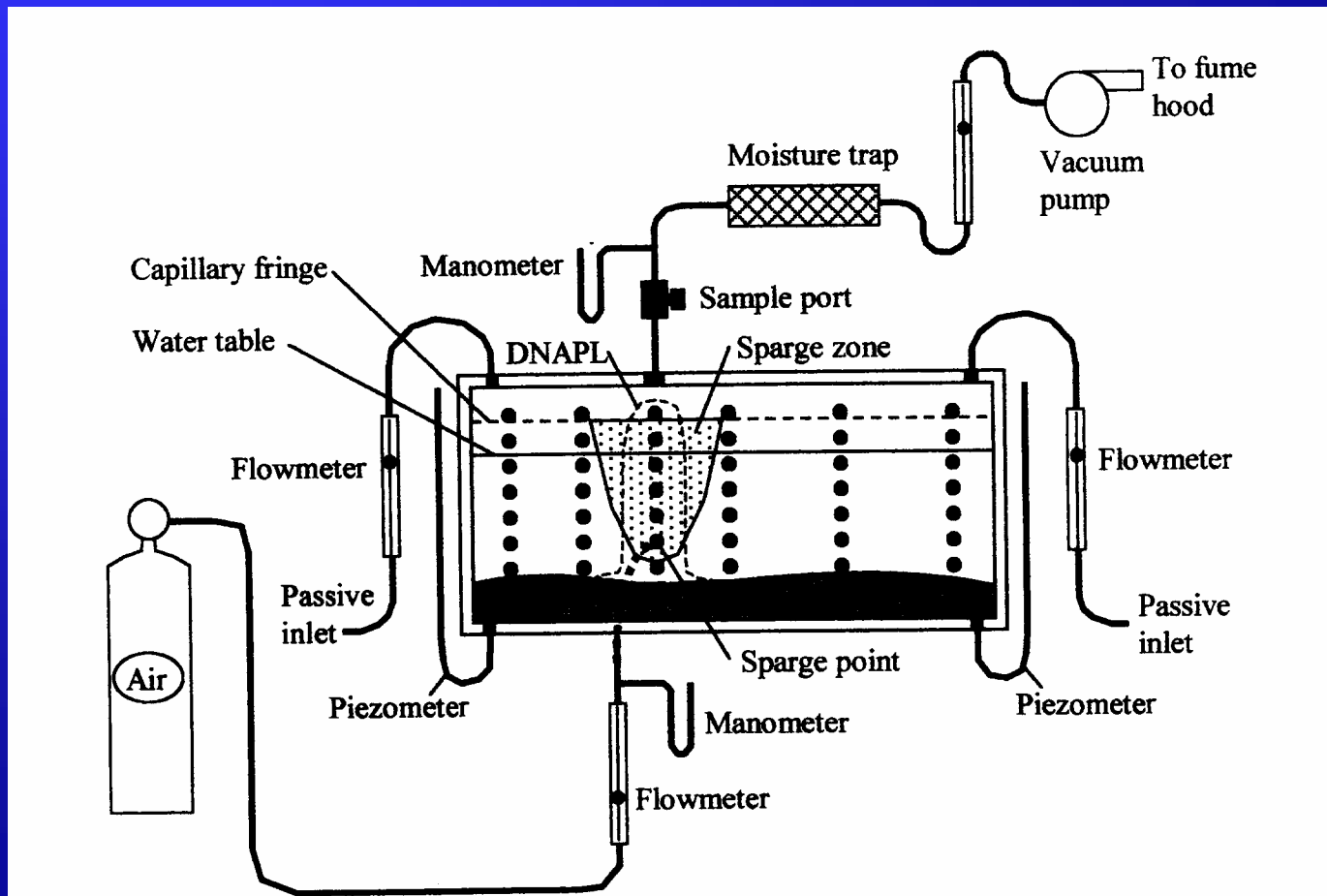
$$Q_{imt} = \underbrace{k_{imt}}_{\text{Mass transfer coefficient}} a (C_w H - C_g)$$

Mass transfer coefficient \times
interfacial area

- Difficult to implement in multiphase flow models due to separate mass balances on each phase of contaminant

*(Braida and Ong, 1998; Elder et al., 1999)

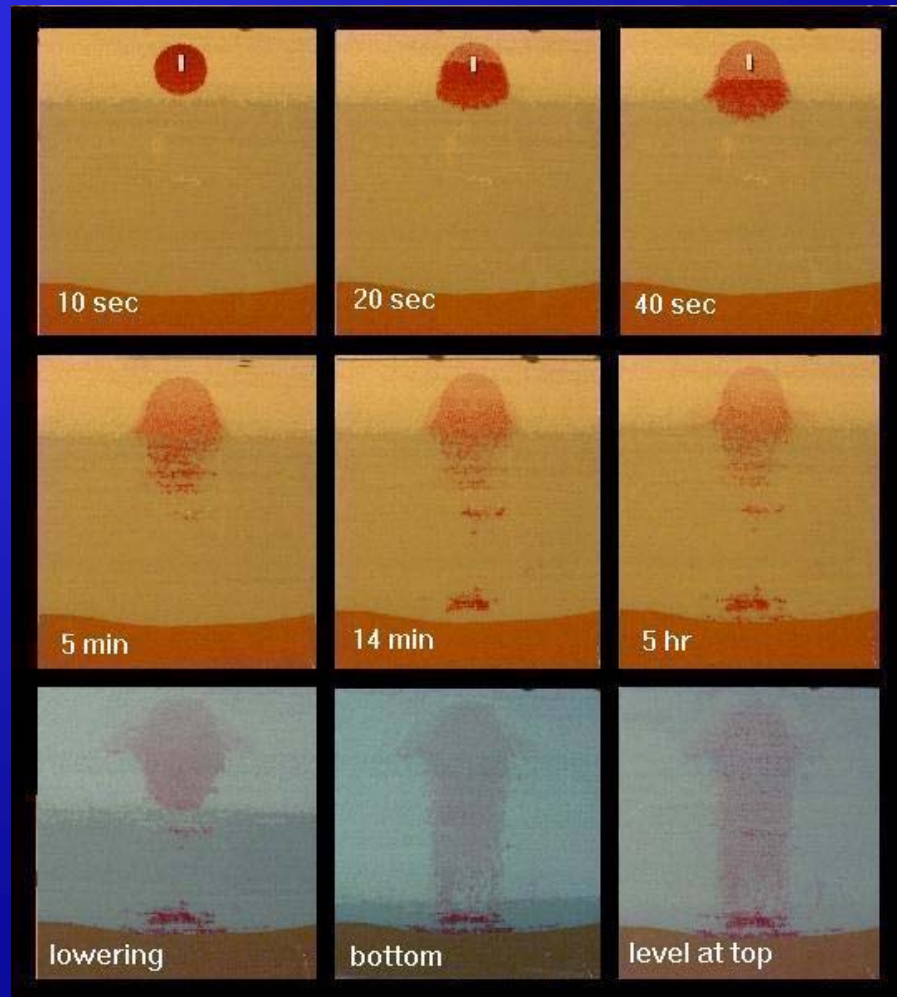
Experiment Set-Up



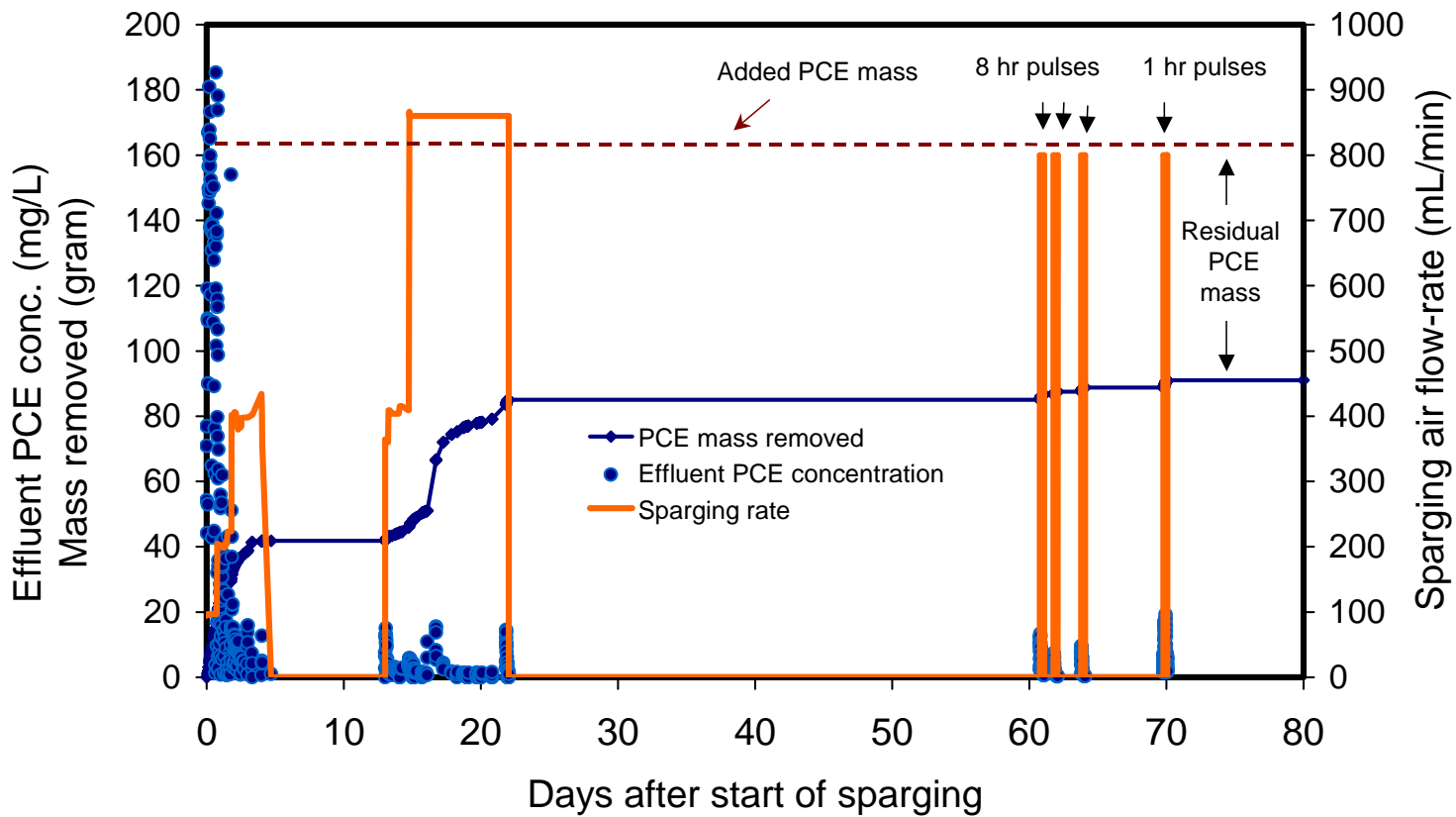
(Heron et al., 2002)

Initial Contaminant Distribution

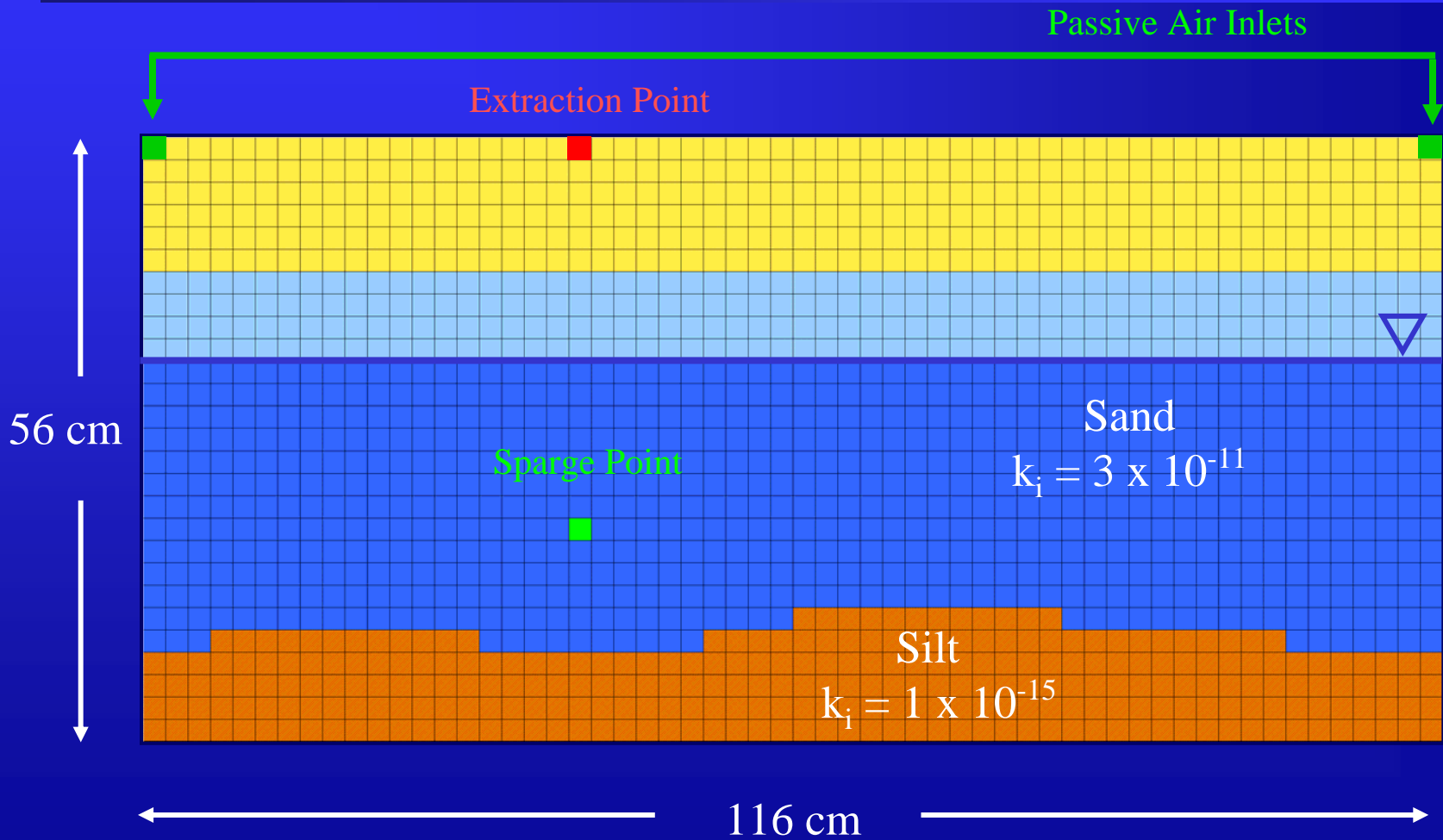
- ★ 100 ml PCE injected
- ★ Water table lowered and raised to vertically smear NAPL



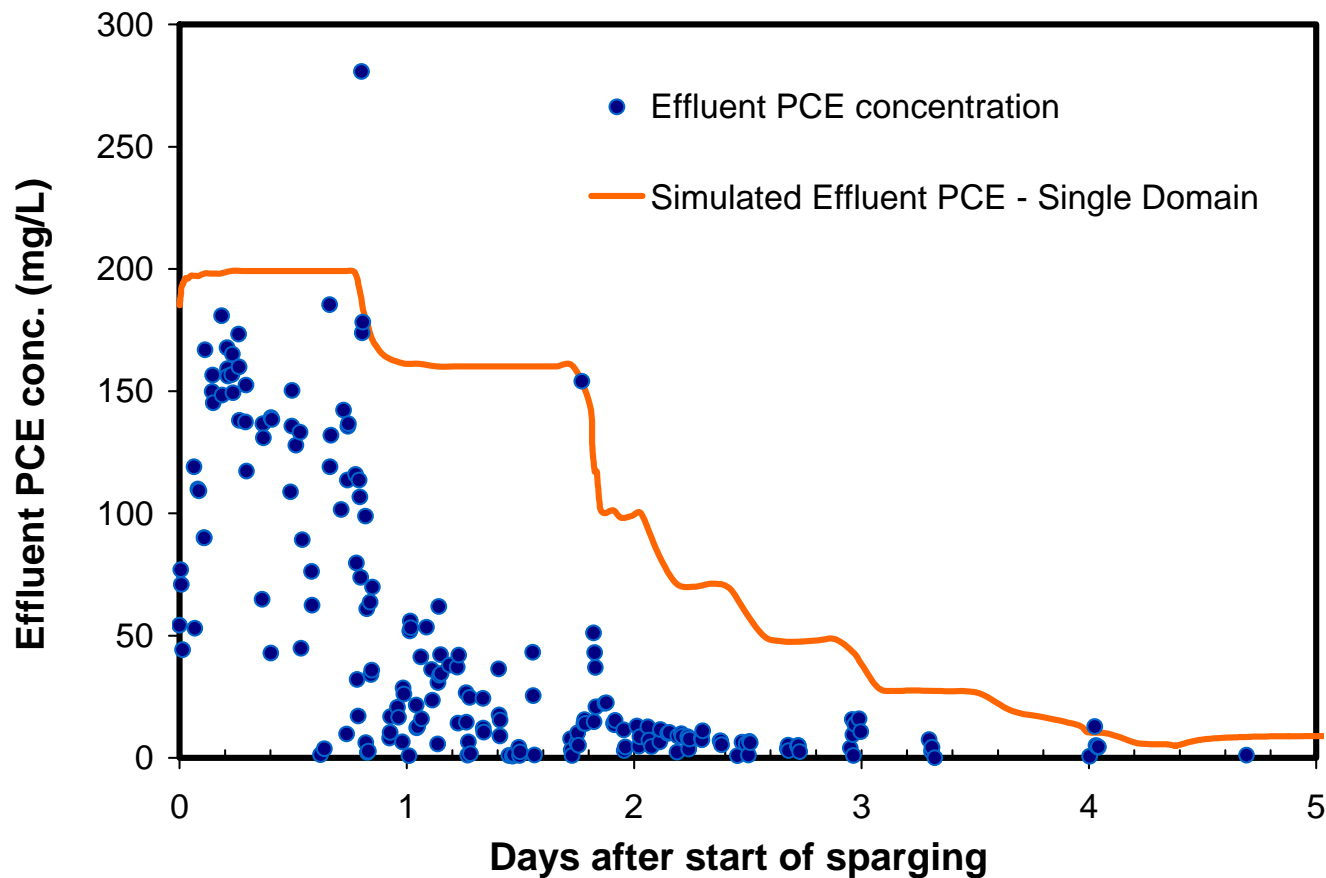
Experiment Data



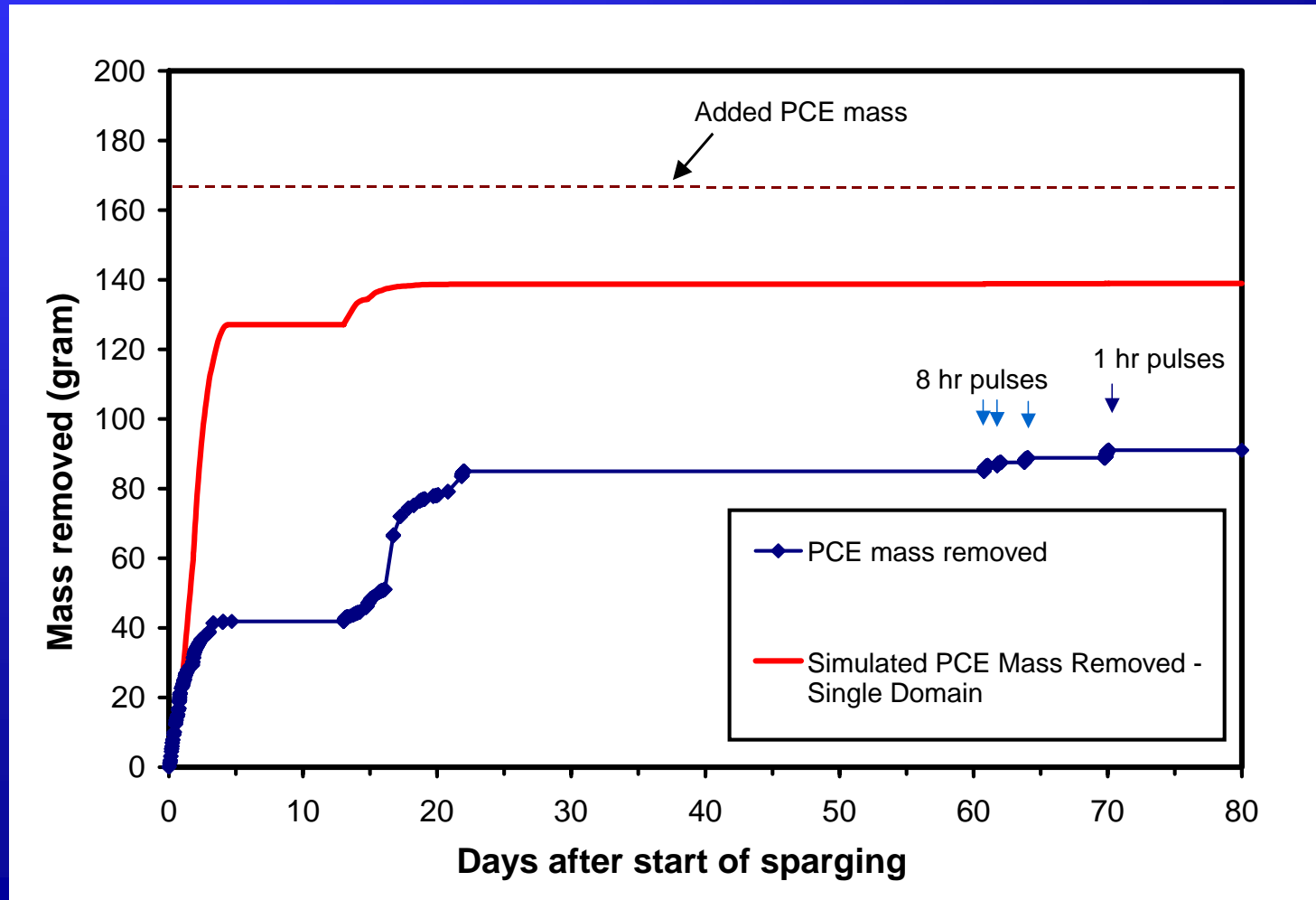
Conceptual Model



Single Domain Simulation Results: Effluent Concentrations



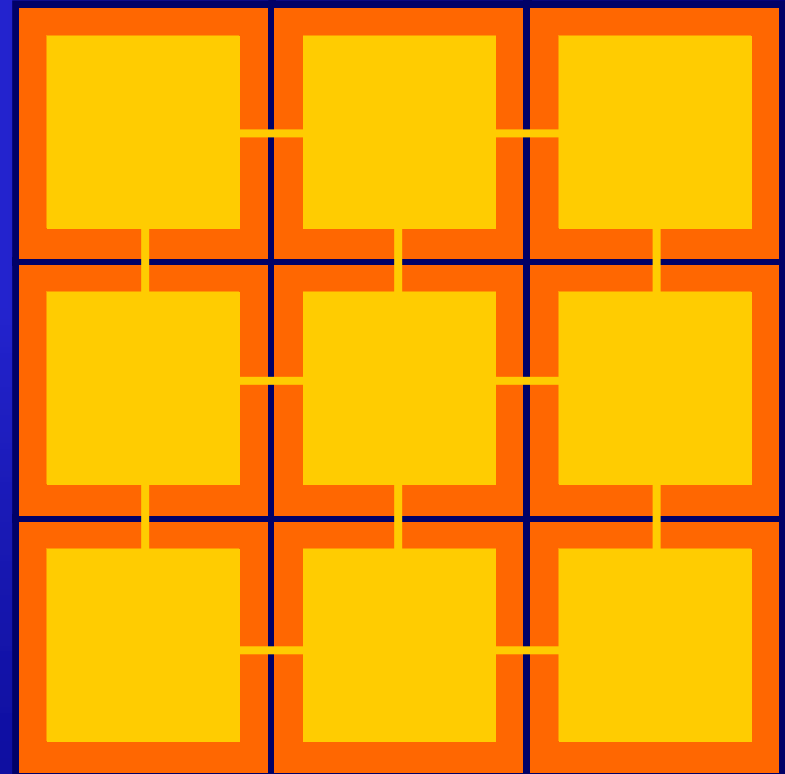
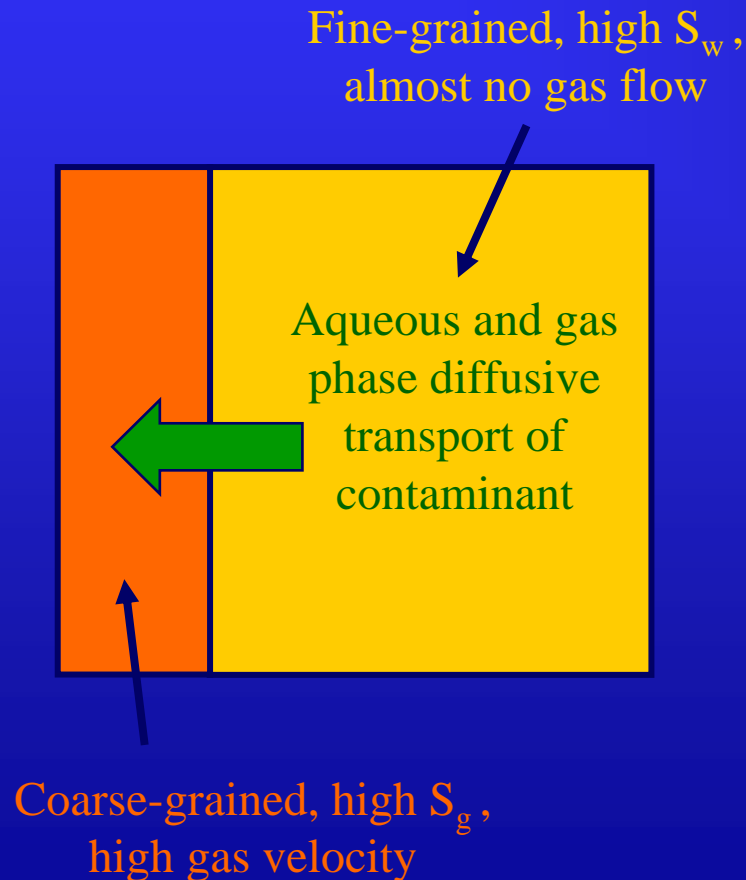
Single Domain Simulation Results: Total Mass Removed



Dual-Domain Approach for Air Sparging*

Conceptual Model

Model Grid

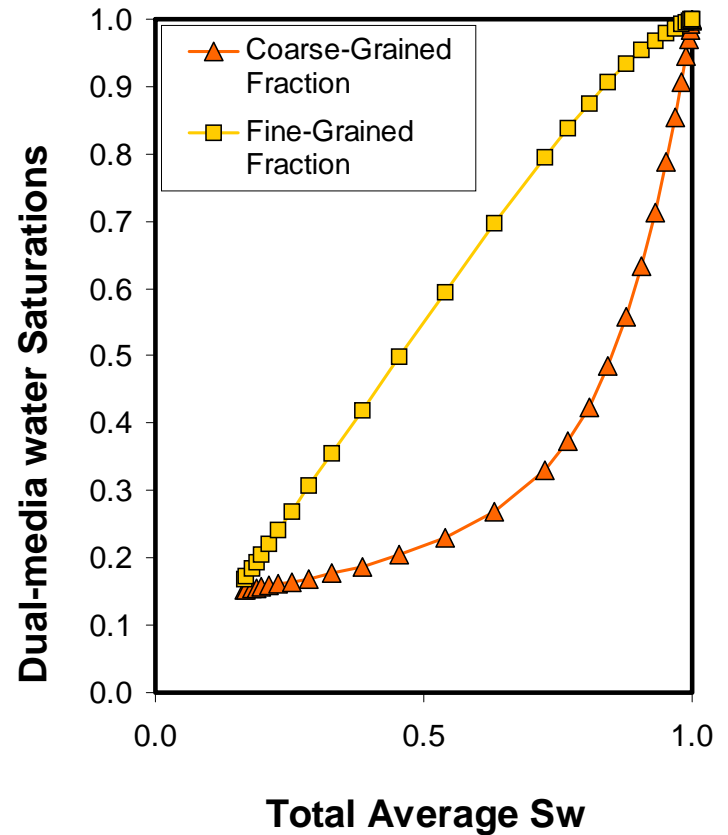
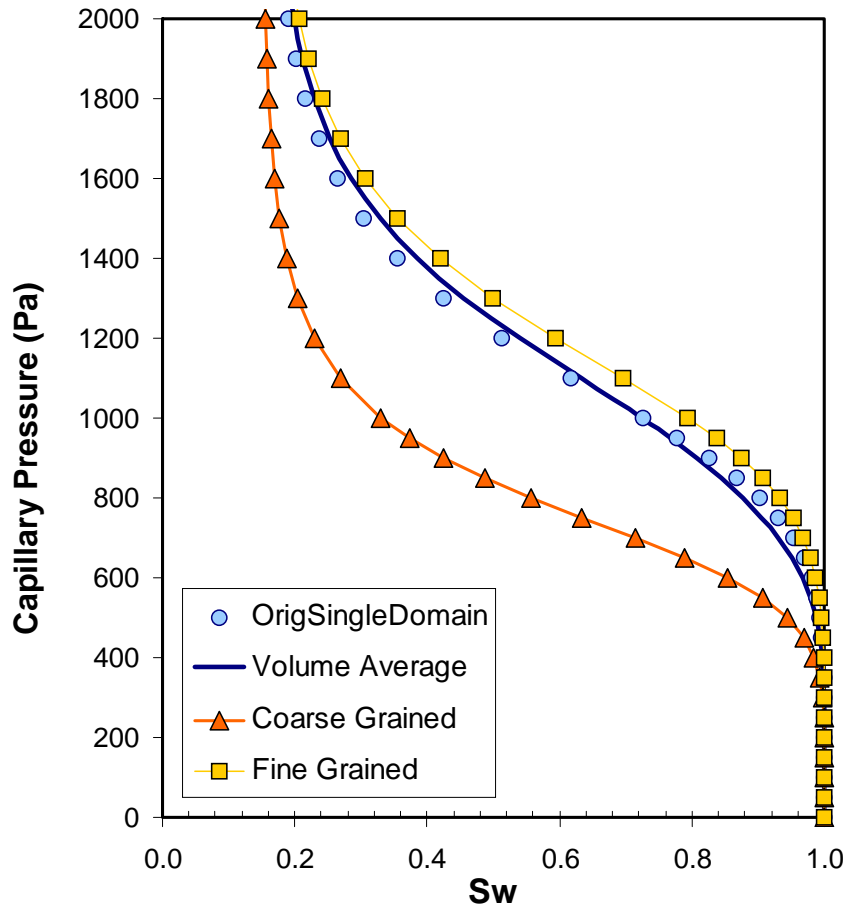


*(Falta, R. W., 2000)

Mass Rate Limitations

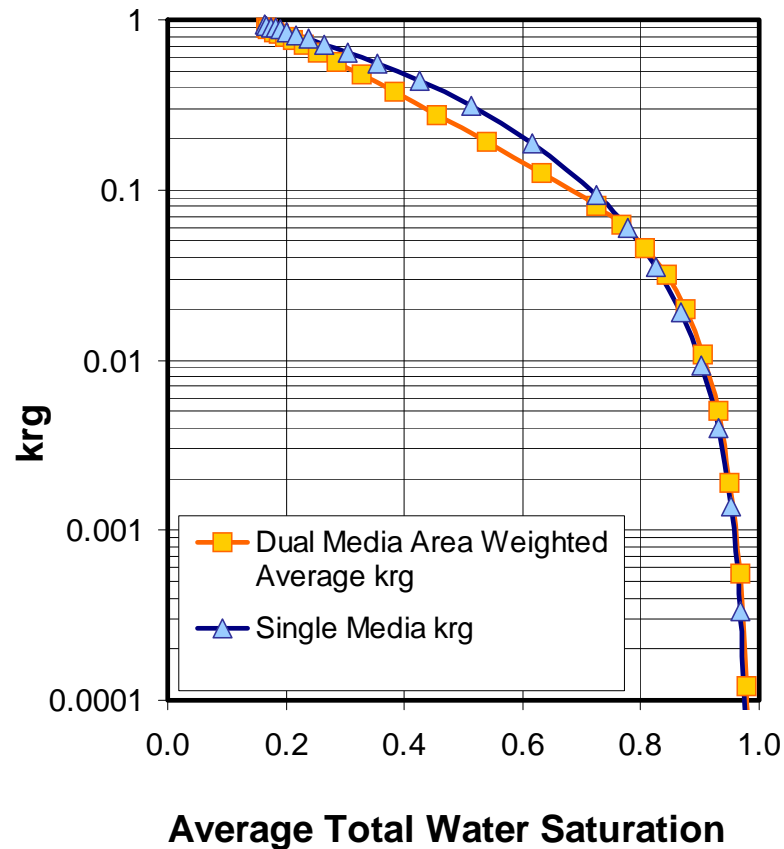
- ★ Accounts for rate-limited mass transfer by:
 - Local equilibrium between flowing gas and porewater within coarse grained fraction
 - 1st order kinetic interphase mass transfer in adjacent fine-grained fraction
- ★ Relative contributions of each region are determined by media volume fractions and water saturation in adjacent media

Dual-Domain Capillary Parameters

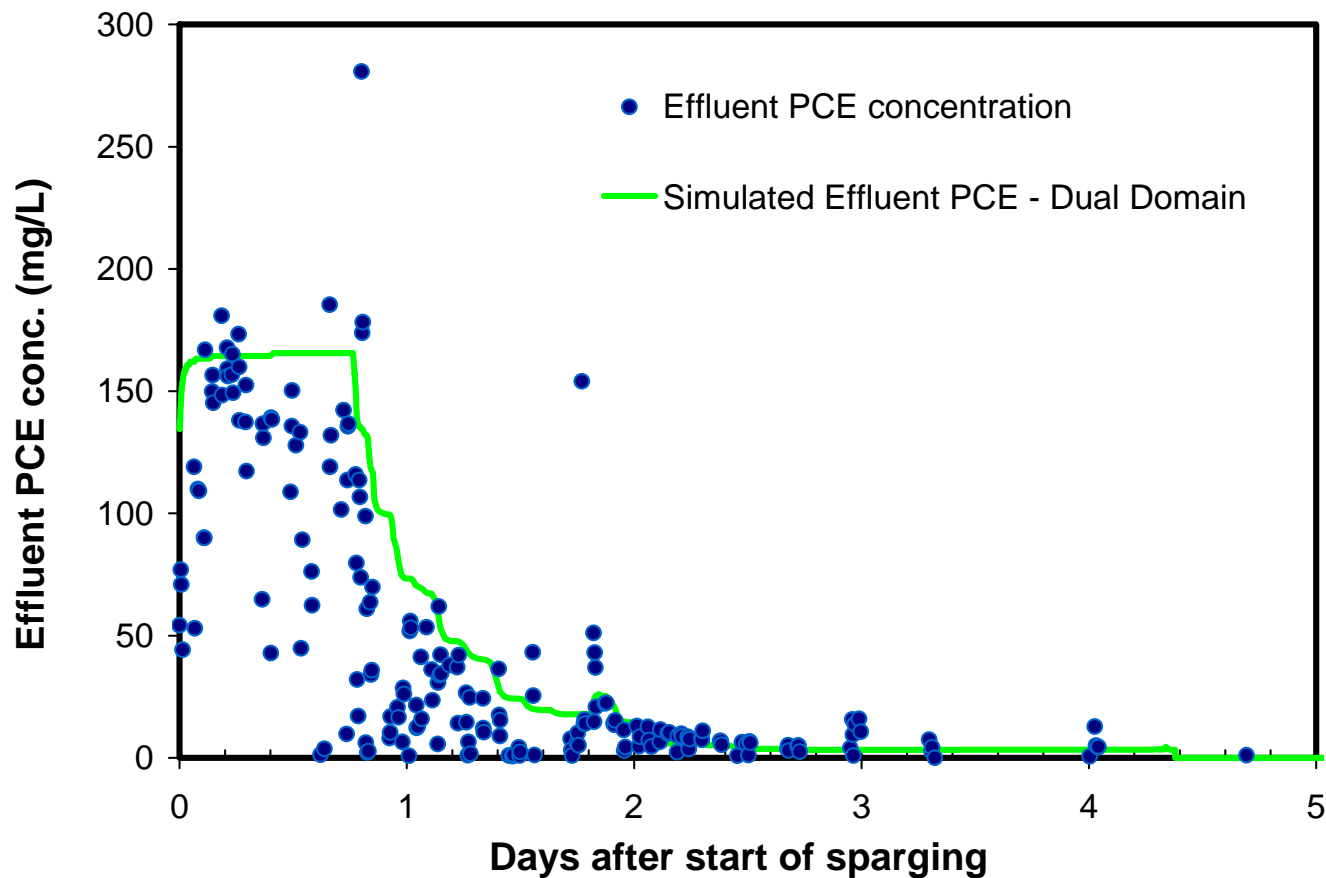


Dual-Domain Relative Permeabilities

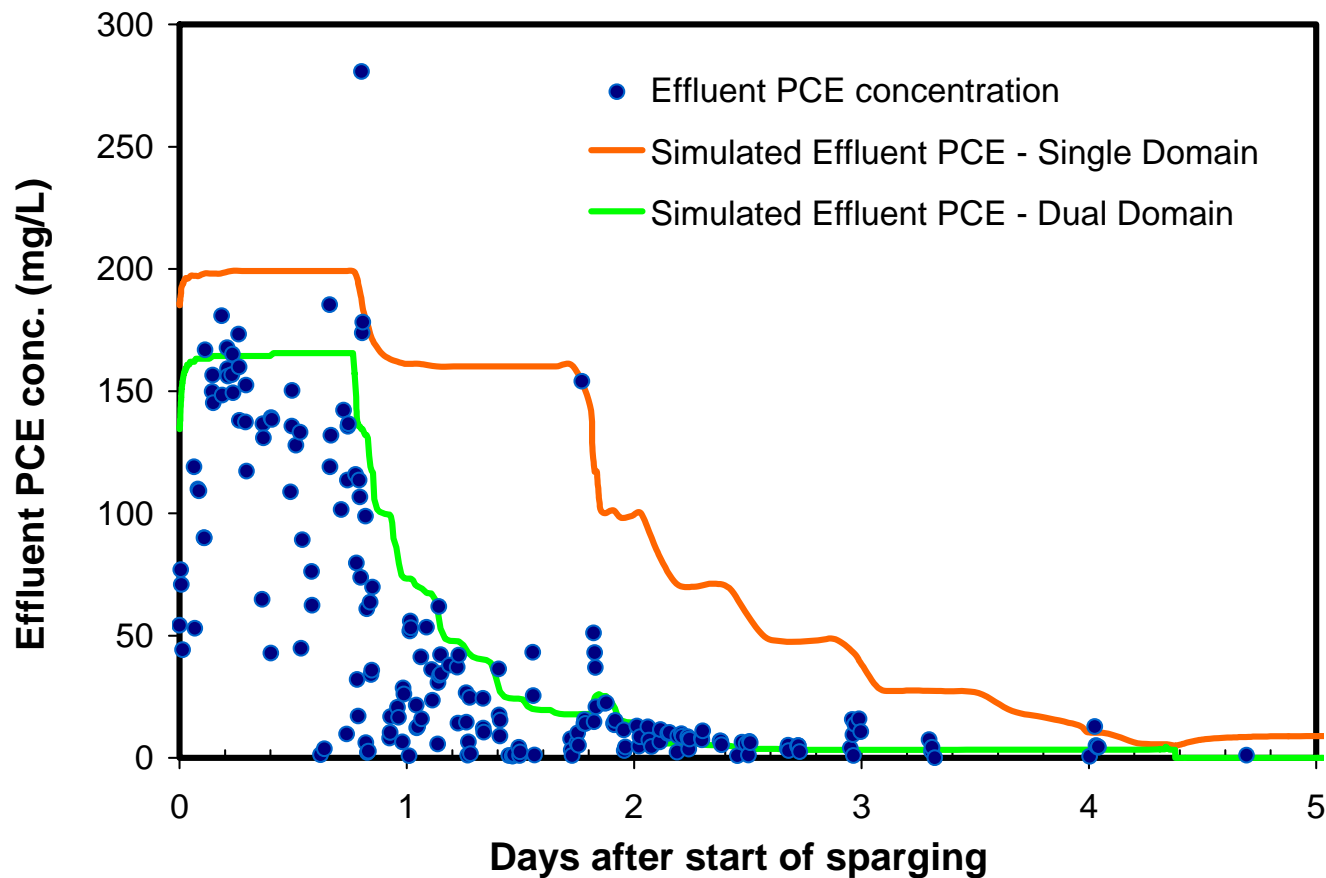
$$k_{rg} = \left(\frac{S_g - S_{gr}}{1 - S_{wr}} \right)^n$$



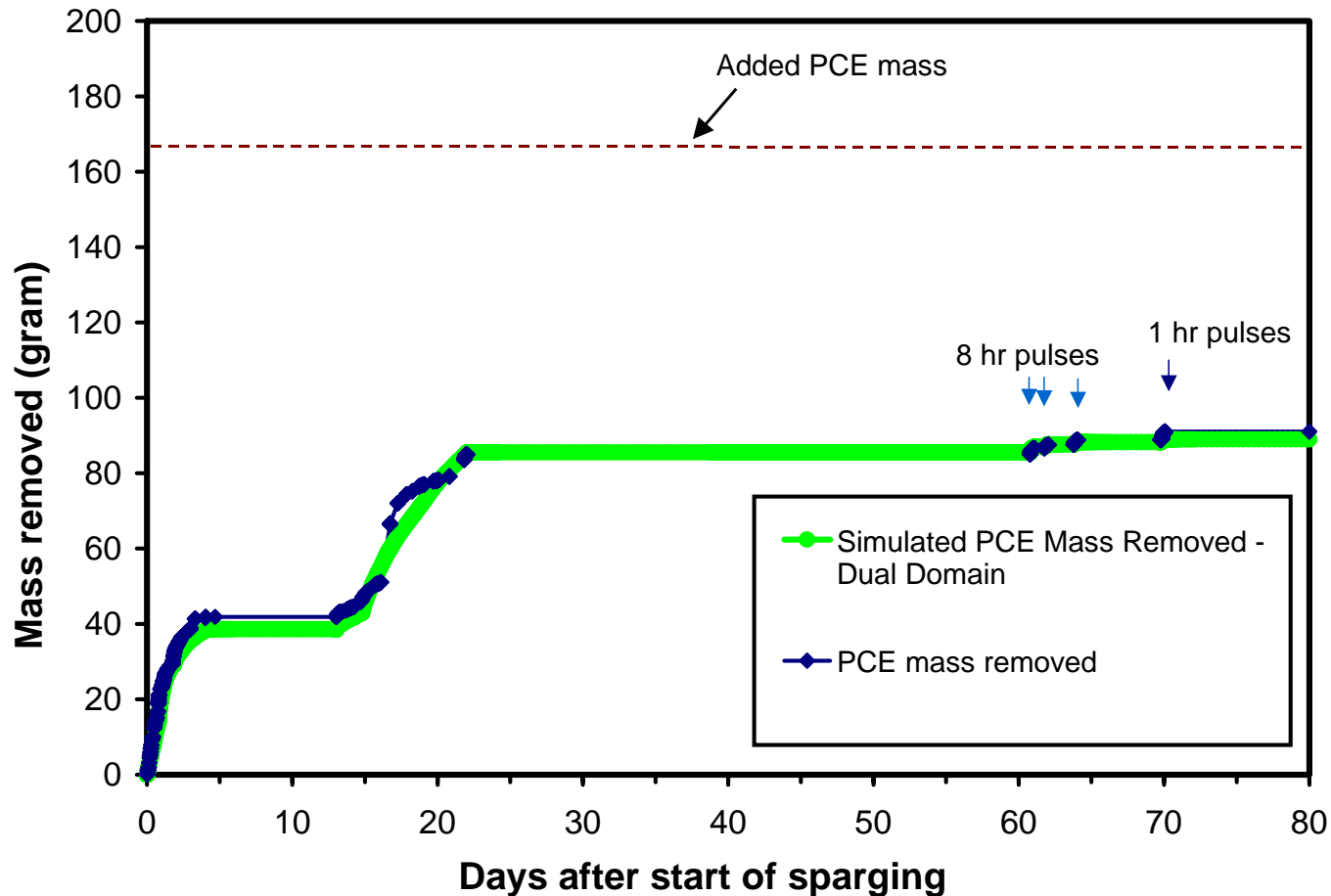
Dual Domain Simulation Results: Effluent Concentrations



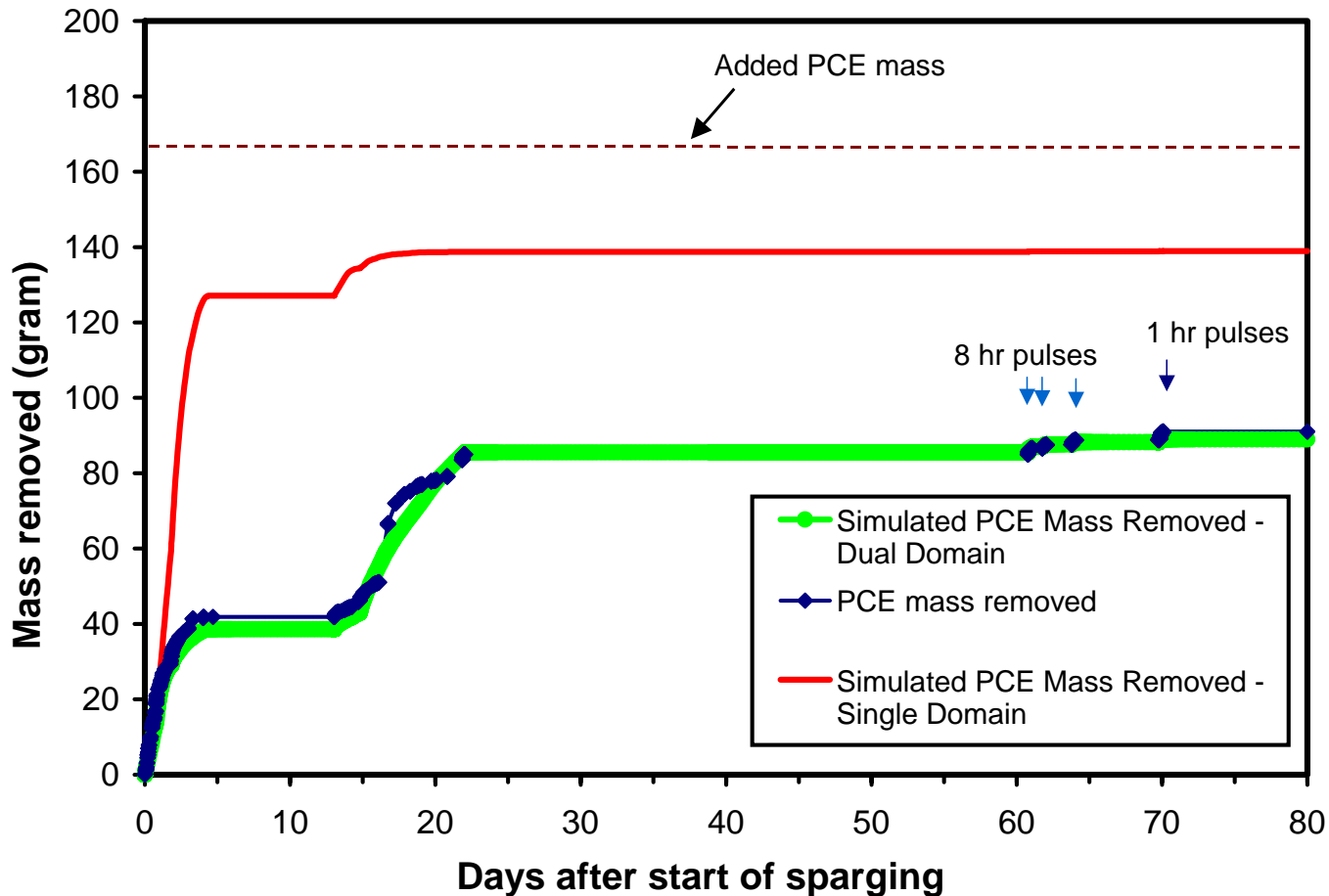
Dual Domain Simulation Results: Effluent Concentrations



Dual Domain Simulation Results: Total Mass Removed



Dual Domain Simulation Results: Total Mass Removed



Summary

- ★ Kinetic interphase mass transfer is an important factor in air sparging mass removal
- ★ T2VOC can be adapted through the dual-domain approach to accurately model rate-limited mass transfer
- ★ Two-dimensional NAPL distribution and aqueous dissolution between pulses being examined
- ★ Field-scale modeling studies need to be performed to assess scale dependency and applicability of method

Acknowledgements

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References:

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Questions??

